Guidelines for Calculating and Reporting Emissions from Bulk Loading Operations

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The purpose of this document is to provide operators with guidelines in estimating emissions from loading of volatile organic containing liquid materials in bulk. Loading losses are the primary source of evaporative emissions that occur as organic vapors in "empty" cargo tanks are displaced to the atmosphere by the liquid being loaded into the tanks. These vapors are a composite of: (1) vapors formed in the empty tank by evaporation of residual product from previous loads, (2) vapors transferred to the tank in vapor balance systems as product is being unloaded, and (3) vapors generated in the tank as the new product is being loaded.

In addition to VOC emissions from evaporative losses, other emissions (NOx, SOx, CO, PM, and toxic air contaminants), from controlling VOC emissions by means of thermal destruction are also expected.

The following guidelines should be used to calculate annual emissions from bulk loading operations. The methodologies assume certain default parameters. Site-specific information should be used, if it is available. There are three emission scenarios for bulk loading operations:

- 1. Simple Operation (No Control)
- 2. Equipped with a Vapor Collection and Recovery System
- 3. Equipped with a Balance System and Vapor Control System

CASE 1) SIMPLE OPERATION (NO VAPOR CONTROL)

$$E_I = Q * L_L Eq. 1$$

Where,

 $E_1 = \text{VOC Emission (un-captured vapor) from Loading Losses}$

Q = Throughput in 1,000 gallons loaded

 L_L = Loading Loss Factor (lbs/1,000 Gallon Loaded) can be found in the Default Emission Factor tables or determined using information dfined in US EPA AP-42, Section 5.2 as follows:

$$L_L = \frac{12.46 \times S \times P \times M}{T}$$

Where,

S =Saturation Factor (see AP-42, Table 5.2-1)

P = True Vapor Pressure, psia

M = Vapor Molecular Weight, lb/lb-mole

T = Temperature of the Liquid being Loaded, °R (°F + 460)

CASE 2) OPERATIONS EQUIPPED WITH VAPOR COLLECTION AND RECOVERY SYSTEMS

Loading emissions from this configuration consist of two parts: 1) uncollected vapor during loading; and 2) collected vapor that was further recovered by the system before exiting the recovery stack.

$$E_2 \; = \; E_{uncollected} \; + \; E_{stack} \; = \; E_{uncollected} \; + \; E_{collected} \; * \; (1 - Eff_{VR})$$

$$E_2 = Q * L_L * (1 - Eff_{VC}) + Q * L_L * Eff_{VC} * (1 - Eff_{VR})$$

$$E_2 = Q * L_L - Q * L_L * Eff_{VC} * Eff_{VR}$$
 Eq. 2

Where,

 E_2 = VOC Emission from Loading Losses

 Eff_{VR} = Vapor Recovery Efficiency (fraction)

 Eff_{VC} = Vapor Collection Efficiency (fraction) as defined in US EPA AP-42, Section 5.2 as follows:

 $Eff_{VC} = 0.992$ for tanker trucks passing MACT-level annual leak test; or

 $Eff_{VC} = 0.987$ for tanker trucks passing the NSPS-level annual leak test; or

 $Eff_{VC} = 0.70$ for tanker trucks not passing either of the above leak tests.

Without specific tests, Vapor Recovery Efficiency (Eff_{VR}) is assumed to be 0.95 and equation 2 becomes:

$$E_2 = Q * L_L * (1 - 0.95 * Eff_{VC})$$
 Eq. 3

CASE 3) OPERATIONS EQUIPPED WITH A VAPOR BALANCE AND DESTRUCTION SYSTEM

Loading emissions from this configuration consisted of two parts: 1) uncollected vapor during loading; and 2) collected vapor that was further recovered by the system before exiting the recovery stack.

$$E_3 = E_{uncollected} + E_{stack} = E_{uncollected} + E_{collected} * (1 - Eff_{VB}) * (1 - Eff_{VD})$$

$$E_3 = Q * L_L * (1 - Eff_{VC}) + Q * L_L * Eff_{VC} * (1 - Eff_{VB}) * (1 - Eff_{VD})$$

$$E_3 = Q * L_L * [1 - Eff_{VC} (Eff_{VB} + Eff_{VD} - (Eff_{VB} * Eff_{VD}))]$$
 Eq. 4

Where,

 E_3 = VOC Emission from Loading Losses

 Eff_{VC} = Vapor Collection Efficiency (fraction) as defined in US EPA AP-42, Section 5.2

 Eff_{VB} = Vapor Balance Efficiency (fraction)

 Eff_{VD} = Vapor Destruction Efficiency (fraction)

A typical system is operating with Vapor Balance Efficiency (Eff_{VB}) of 50% (or 0.50). Without specific tests, Vapor Destruction Efficiency (Eff_{VD}) is assumed to be 99% (or 0.99) and equation 4 becomes:

$$E_3 = Q * L_L * (1 - 0.995 * Eff_{VC})$$
 Eq. 5

THERMAL OXIDATION

If the operation is equipped with a VOC destruction system by means of thermal oxidation, other contaminants (NOx, SOx, CO, PM, and toxic air contaminants) resulted from burning off organic vapor are expected. AQMD encourages operators to use test results to calculate and report emissions. Since the organic vapor evaporates from loading of liquid organic materials, the captured for control vapor must be converted back into liquid form for consistency in emission calculations. The AQMD uses an equivalent method to determine the throughput of vapors directed to a thermal oxidizer (TO) as equivalent 1000 of gallons of liquid (Mgal).

$$TO_{Throughput} = \frac{E_{collected}}{1,000 * d_I} * (1 - Eff_{VB})$$

$$TO_{Throughput} = \frac{Q * L_L * Eff_{VC}}{1,000 * d_L} * (1 - Eff_{VB})$$
 Eq. 6

A typical system is operating with Vapor Balance Efficiency (Eff_{VB}) of 50% (or 0.50). Throughput for the TO become:

$$TO_{Throughput} = 0.0005 * Eff_{VC} * \frac{Q * L_L}{d_l}$$
 Eq. 7

Where, d_l is the liquid density.

EXAMPLES

The following examples will demonstrate how emissions are calculated for a typical bulk loading operation in all three cases. The examples also included images of screens for how to report emissions under the new reporting system.

CASE 1 - SIMPLE OPERATION (NO VAPOR CONTROL)

Company XYZ splash loaded 120,000 gallons of gasoline RVP 10 at the following conditions:

S = 1.45 (Saturation Factor from AP-42)

T = 70°F = 530°R (Temperature of Gasoline)

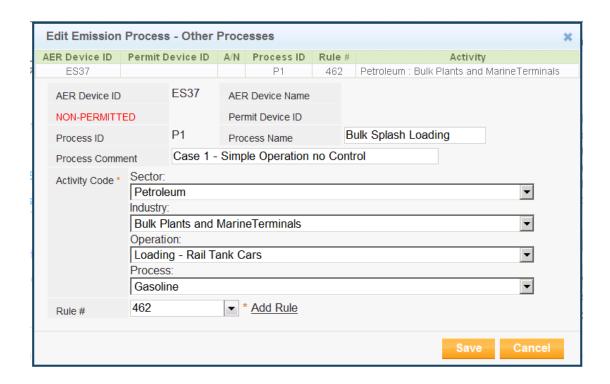
P = 6.2 psia (True Vapor Pressure)

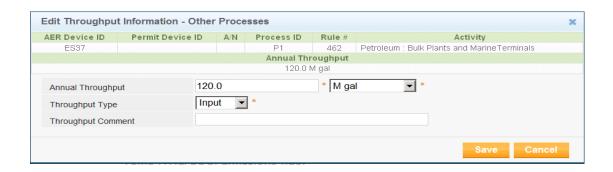
M = 66 lb/lb-mole (Vapor Molecular Weight)

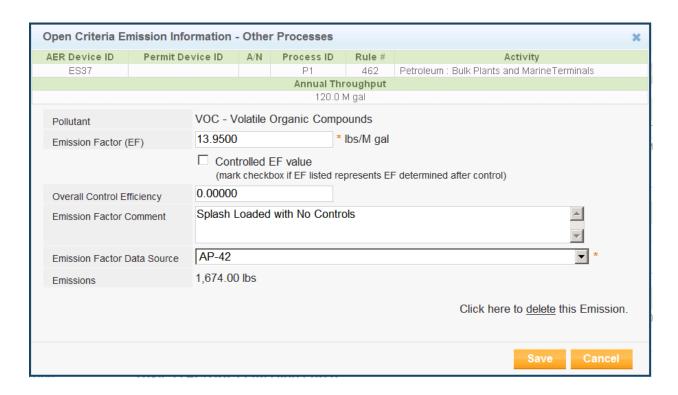
$$L_L = \frac{12.46 \times S \times P \times M}{T} = \frac{12.46 \times 1.45 \times 6.2 \times 66}{530} = 13.95 \ lbs \ VOC/Mgal$$

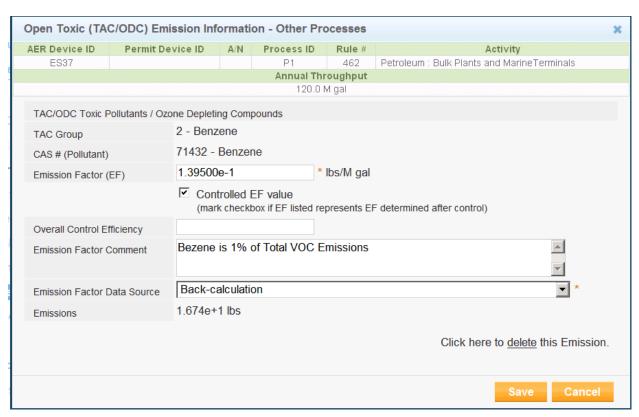
Equation 1 yields the VOC emissions as follows:

$$E_1 = 120 Mgals * 13.95 \frac{lbs VOC}{Mgal} = 1,674 lbs VOC$$









CASE 2 - OPERATIONS EQUIPPED WITH VAPOR COLLECTION AND RECOVERY SYSTEMS

Company ABC operates a loading terminal with vapor balance service with submerged bottom filling technology into tanker trucks that have passed the MACT level leak test. The vapor vent line is connected to a refrigeration unit that recovers 95% of the vapor and returns it back as liquid to storage tank. ABC transferred 1,000,000 gallons of RVP 10 gasoline over the year at the following conditions:

S = 1.0 (Saturation Factor from AP-42)

T = 70° F = 530° R (Temperature of Gasoline)

P = 6.2 psia (True Vapor Pressure)

M = 66 lb/lb-mole (Vapor Molecular Weight)

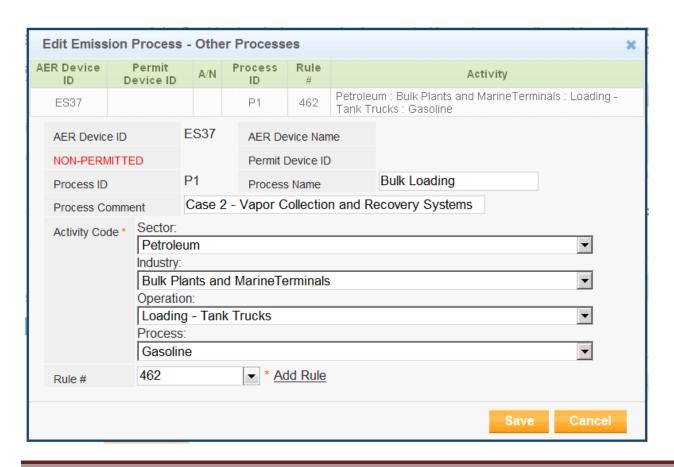
 $Eff_{VR} = 0.95$ (Vapor Recovery Efficiency)

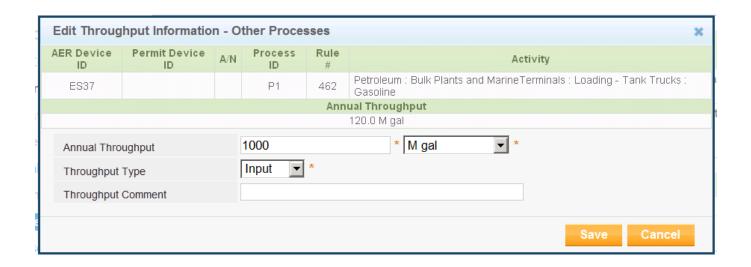
 $Eff_{VC} = 0.992$ (Vapor Collection Efficiency)

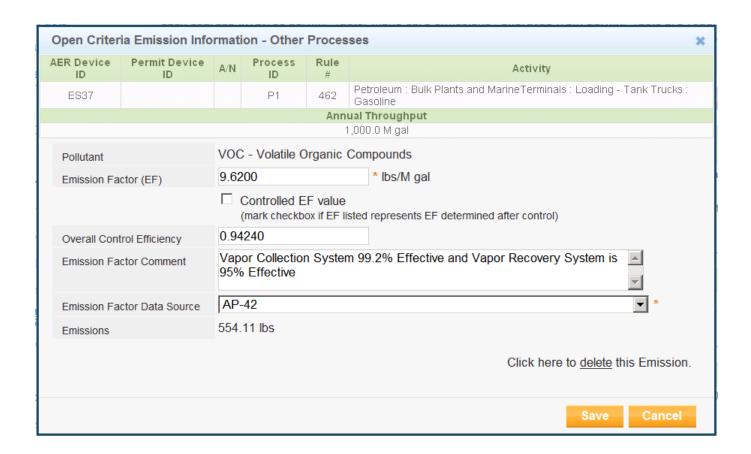
$$L_L = \frac{12.46 \times S \times P \times M}{T} = \frac{12.46 \times 1 \times 6.2 \times 66}{530} = 9.62 \ lb \ VOC/Mgal$$

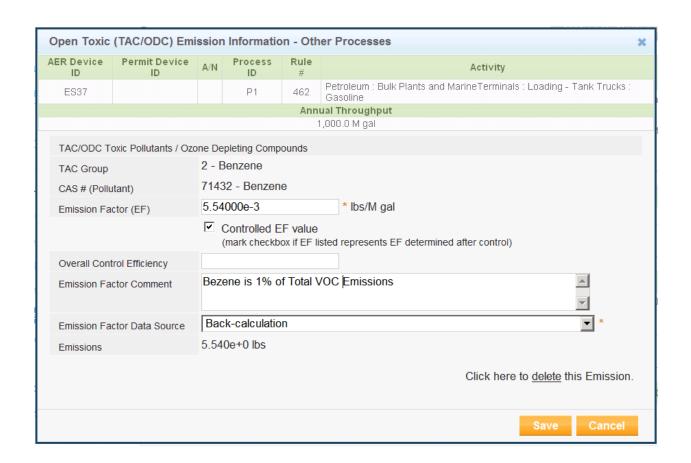
Equation 3 yields the VOC emissions as follows:

$$E_2 = 1,000 \, Mgals * 9.62 \, \frac{lbs \, VOC}{Mgal} * (1 - 0.95 * 0.992) = 554 \, lbs \, VOC$$









CASE 3 - OPERATIONS EQUIPPED WITH A VAPOR BALANCE AND DESTRUCTION SYSTEM

Over the year, company RST operates a loading terminal with submerged bottom filling 125,000,000 gallons of gasoline RVP 10 into tanker trucks that have passed the MACT level leak test at the same conditions as Case 2. The vapor vent line is connected to a system of vapor balance and then to an afterburner (thermal oxidizer -TO). The system of vapor balance achieves an overall efficiency of 49%. The oxidizer operates at 99.4% destruction efficiency.

 $L_L = 9.62 lb VOC/Mgal$ (see Case 2 studies for loading loss factor calculation)

Q = 125,000 Mgals

 $Eff_{VC} = 0.992$ (Vapor Collection Efficiency)

 $Eff_{VB} = 0.49$ (Vapor Balance Efficiency)

 $Eff_{VD} = 0.994$ (Vapor Destruction Efficiency)

Equation 4 yields the VOC emissions as follows:

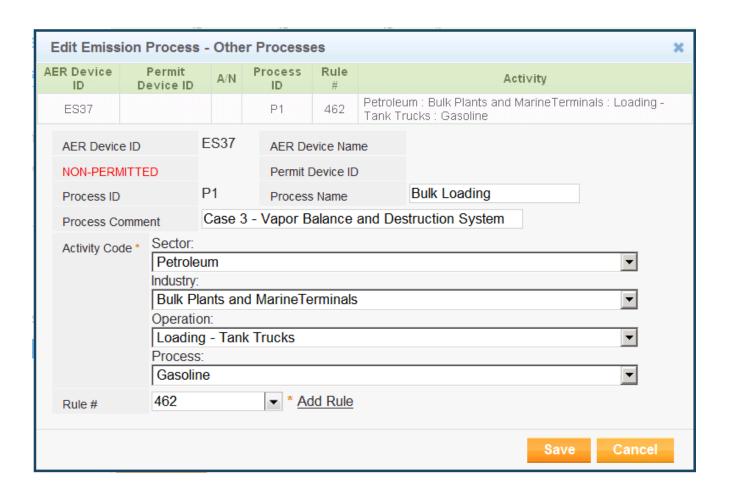
$$E_3 = 125,000 \, Mgals * 9.62 \, \frac{lbs \, VOC}{Mgal} * [1 - 0.992 * (0.49 + 0.994 - (0.49 * 0.994))] = 13,276 \, lbs \, VOC$$

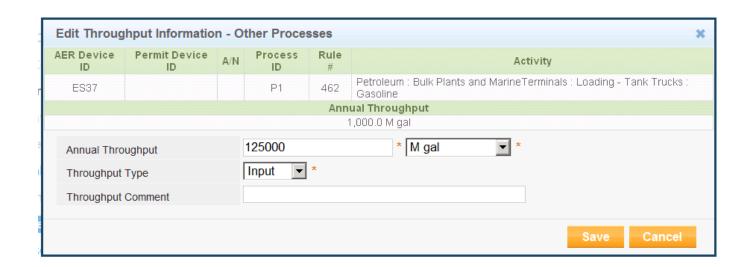
COMBUSTION EMISSIONS FROM THERMAL OXIDIZER (TO)

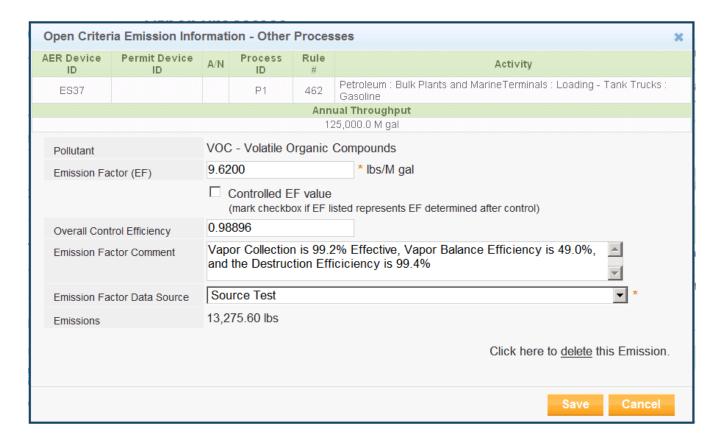
All thermal oxidizers used at bulk loading facilities are required to have a CARB Certification Test. In some cases, NOx, SOx, CO, and PM emission rates are tested and determined in terms of lbs of pollutant/Mgal material loaded. AQMD encourages operator to use the test results in calculating and reporting emissions.

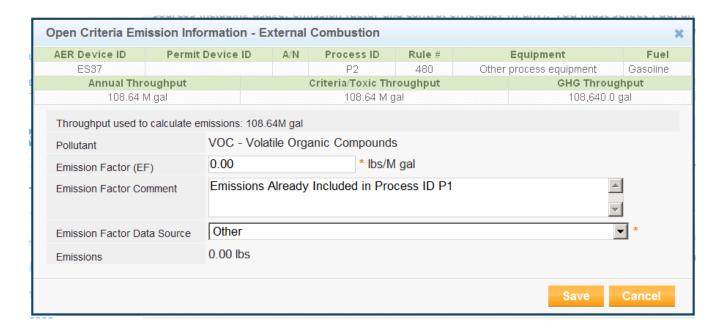
In this example, other contaminants were not tested for the TO. Emissions for other air contaminants are calculated using the best available default factors published in AER Program Help & Support. Throughput for the TO is determined using Equation 5 as follows for gasoline RVP 10 with liquid density of 5.6 lbs/gallon:

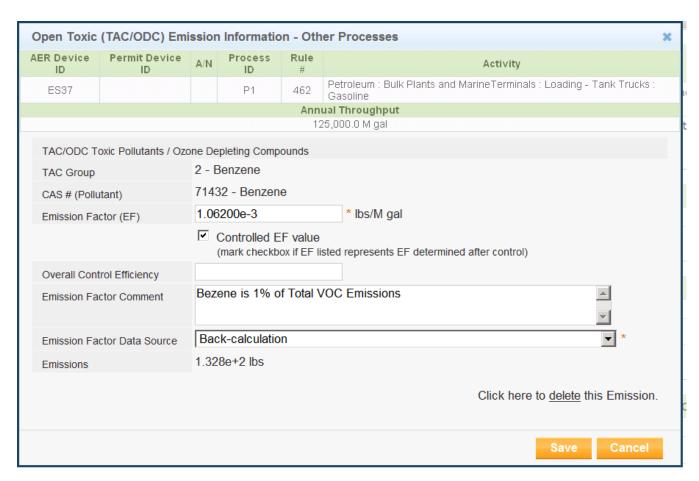
$$TO_{Throughput} = \frac{125,000 * 9.62 * 0.992}{1,000 * 5.6} * (1 - 0.49) = 108.64 Mgals of gasoline$$

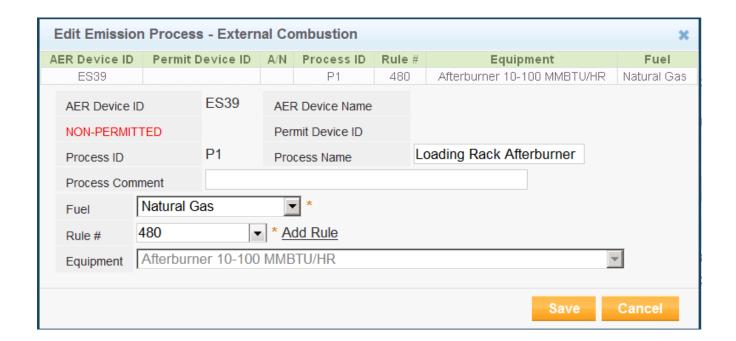


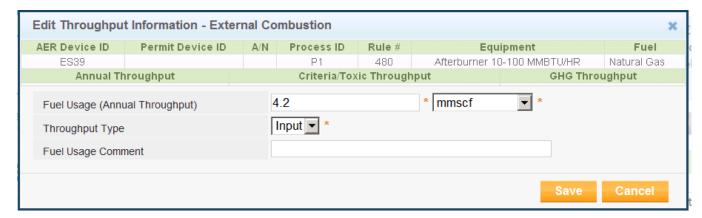












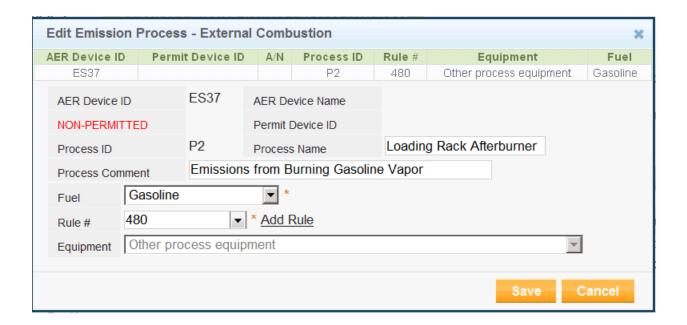
Report Criteria and toxic compounds using default factors as below:

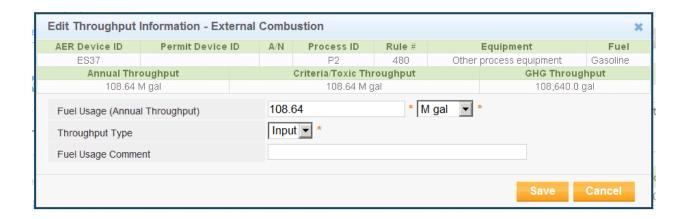
Criteria Emissions (lbs)

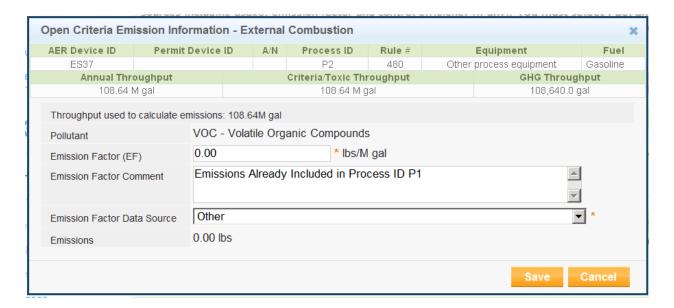
	Pollutant	EF	Unit	EF Data Source	Overall CE	Emissions
<u>Open</u>	VOC	7.00	lbs / mmscf	AQMD default		29.40
<u>Open</u>	NOx	130.00	lbs / mmscf	AQMD default		546.00
<u>Open</u>	SOx	0.60	lbs / mmscf	AQMD default		2.52
<u>Open</u>	CO	35.00	lbs / mmscf	AQMD default		147.00
<u>Open</u>	PM	7.50	lbs / mmscf	AQMD default		31.50

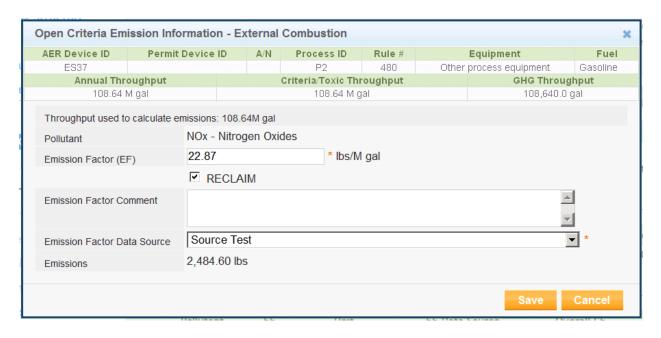
Toxic (TAC/ODC) Emissions (lbs)

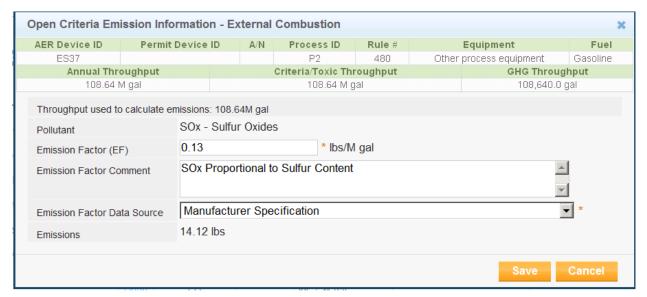
	TAC/ODC Group	CAS #	EF	Unit	EF Data Source	Overall CE	Emissions
<u>Open</u>	Benzene	71432	5.80000e-3	lbs / mmscf	AQMD default		2.436e-2
<u>Open</u>	Formaldehyde	50000	1.23000e-2	lbs / mmscf	AQMD default		5.166e-2
<u>Open</u>	PAHs [PAH, POM]	1151	1.00000e-4	lbs / mmscf	AQMD default		4.200e-4
<u>Open</u>	PAHs [PAH, POM]	91203	3.00000e-4	lbs / mmscf	AQMD default		1.260e-3
<u>Open</u>	Acetaldehyde	75070	3.10000e-3	lbs / mmscf	AQMD default		1.302e-2
<u>Open</u>	Acrolein	107028	2.70000e-3	lbs / mmscf	AQMD default		1.134e-2
<u>Open</u>	Ammonia	7664417	1.80000e+1	lbs / mmscf	AQMD default		7.560e+1
<u>Open</u>	Ethyl benzene	100414	6.90000e-3	lbs / mmscf	AQMD default		2.898e-2
<u>Open</u>	Hexane	110543	4.60000e-3	lbs / mmscf	AQMD default		1.932e-2
<u>Open</u>	Toluene	108883	2.65000e-2	lbs / mmscf	AQMD default		1.113e-1
<u>Open</u>	Xylenes	1330207	1.97000e-2	lbs / mmscf	AQMD default		8.274e-2
Add New							

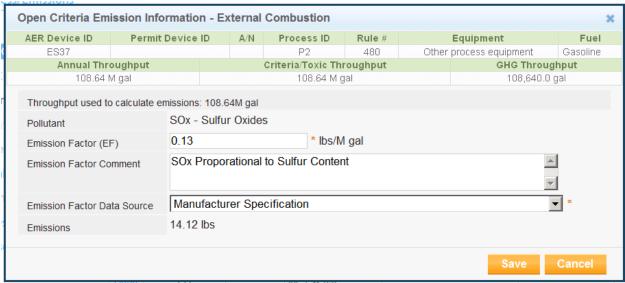


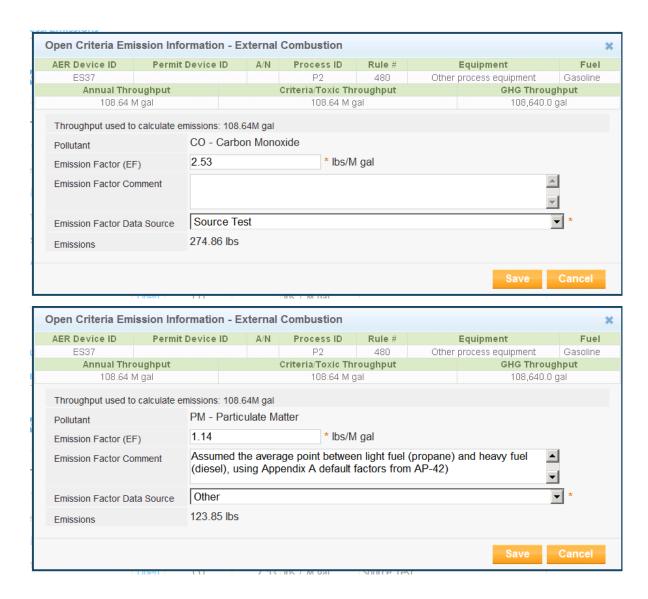












Facilities must report toxic emission as well for this process. If default emission factors are needed, use the following, in pounds/1000 gallons of equivalent gasoline burned.

POLLUTANT	CAS NO.	EMISSION FACTOR	
Benzene	71432	3.8061	
1,3-Butadiene	106990	0.3240	
Formaldehyde	50000	3.4520	
Nickel	7440020	0.0033	
PAHs	1151	0.1438	